I. CLAIMS

1. (Original) An electrochemical fuel cell comprising first and second monolithic electrically

conducting flow field-bipolar plate assemblies arranged essentially parallel to each other such

that an inside surface of the first flow field-bipolar plate assembly is facing an inside surface of

the second flow field-bipolar plate assembly, wherein the flow field-bipolar plate assemblies are

electrically and mechanically connected by intervening layers, the intervening layers comprising:

a first electrically conducting intermediate layer bonded directly to the inside surface of

the first flow field-bipolar plate assembly,

a second electrically conducting intermediate layer bonded directly to the inside surface

of the second flow field-bipolar plate assembly,

a first electrode bonded directly to the inside surface of the first electrically conducting

intermediate layer,

a second electrode bonded directly to the inside surface of the second electrically

conducting intermediate layer, and

a polymer electrolyte membrane between and bonded directly to both of the electrodes.

2. (Original) The electrochemical fuel cell of claim 1, wherein the monolithic flow field-bipolar

plate assemblies comprise a first and second porous metal flow field directly bonded to opposite

sides of an electrically conducting gas barrier by continuous metallurgical bonds.

3. (Original) The electrochemical fuel cell of claim 2, wherein the porous metal flow fields are

directly bonded to the electrically conducting gas barrier by electroplating or sintering.

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4. (Original) The electrochemical fuel cell of claim 2, wherein the electrically conducting gas

barrier comprises a metal foil.

5. (Original) The electrochemical fuel cell of claim 2, wherein at least one porous metal flow

field comprises a three-dimensional reticulated metal structure.

6. (Original) The electrochemical fuel cell of claim 2, wherein at least one porous metal flow

field further comprises a protecting layer disposed on at least one surface thereof.

7. (Original) The electrochemical fuel cell of claim 6, wherein the protecting layer comprises a

metal or a metal oxide.

8. (Original) The electrochemical fuel cell of claim 7, wherein the protecting layer is a

continuous layer of tin oxide.

9. (Original) The electrochemical fuel cell of claim 1, wherein the intermediate layer comprises

a polymer and high surface area carbon particles.

10. (Original) The electrochemical fuel cell of claim 9, wherein the polymer comprises

polytetrafluoroethylene, perfluoroethylene-perfluoropropylene copolymer, perfluoro-alkoxy, or

polyvanilidene fluoride.

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11. (Original) The electrochemical fuel cell of claim 1, wherein the electrode comprises a

polymer electrolyte and an electrocatalyst.

12. (Original) The electrochemical fuel cell of claim 1, wherein at least one of the flow field-

bipolar plate assemblies comprises a first metal flow field directly bonded to the outside surface

of an electrically conducting gas impermeable barrier, a second porous metal flow field directly

bonded to the outside surface of a second electrically conducting gas impermeable barrier, and a

porous metal cooling field disposed between and directly bonded to the inside surfaces of the

first and second gas impermeable barriers.

13. (Original) An electrochemical fuel cell stack comprising two electrically conducting end-

plates and a plurality of electrochemical fuel cells disposed between the endplates, wherein the

electrochemical fuel cells comprise first and second monolithic electrically conducting flow

field-bipolar plate assemblies arranged essentially parallel to each other such that an inside

surface of the first flow field-bipolar plate assembly is facing an inside surface of the second

flow field-bipolar plate assembly, wherein the flow field-bipolar plate assemblies are electrically

and mechanically connected by intervening layers, the intervening layers comprising:

a first electrically conducting intermediate layer bonded directly to the inside surface of

the first flow field-bipolar plate assembly,

a second electrically conducting intermediate layer bonded directly to the inside surface

of the second flow field-bipolar plate assembly,

a first electrode bonded directly to the inside surface of the first electrically conducting

intermediate layer,

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a second electrode bonded directly to the inside surface of the second electrically

conducting intermediate layer, and

a polymer electrolyte membrane between and bonded directly to both of the electrodes.

14. (Original) A method of making a fuel cell stack comprising disposing between two

electrically conducting endplates a plurality of electrochemical fuel cells, wherein the

electrochemical fuel cells comprise first and second monolithic electrically conducting flow

field-bipolar plate assemblies arranged essentially parallel to each other such that an inside

surface of the first flow field-bipolar plate assembly is facing an inside surface of the second

flow field-bipolar plate assembly, wherein the flow field-bipolar plate assemblies are electrically

and mechanically connected by intervening layers, the intervening layers comprising:

a first electrically conducting intermediate layer bonded directly to the inside surface of

the first flow field-bipolar plate assembly,

a second electrically conducting intermediate layer bonded directly to the inside surface

of the second flow field-bipolar plate assembly,

a first electrode bonded directly to the inside surface of the first electrically conducting

intermediate layer,

a second electrode bonded directly to the inside surface of the second electrically

conducting intermediate layer, and

a polymer electrolyte membrane disposed between and bonded directly to both of the

electrodes.

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09/779,872 Page 5 of 8 15. (Original) A method of generating electrical power comprising supplying hydrogen and

oxygen to an electrochemical fuel cell stack,

wherein the electrochemical fuel cell stack comprises two electrically conducting end-

plates and a plurality of electrochemical fuel cells disposed between the endplates; wherein the

electrochemical fuel cells comprise first and second monolithic electrically conducting flow

field-bipolar plate assemblies arranged essentially parallel to each other such that an inside

surface of the first flow field-bipolar plate assembly is facing an inside surface of the second

flow field-bipolar plate assembly, wherein the flow field-bipolar plates assemblies are

electrically and mechanically connected by intervening layers, the intervening layers comprising:

a first electrically conducting intermediate layer bonded directly to the inside surface of

the first flow field-bipolar plate assembly,

a second electrically conducting intermediate layer bonded directly to the inside surface

of the second flow field-bipolar plate assembly,

a first electrode bonded directly to the inside surface of the first electrically conducting

intermediate layer,

a second electrode bonded directly to the inside surface of the second electrically

conducting intermediate layer, and

a polymer electrolyte membrane between and bonded directly to both of the electrodes.

16. -42. (Cancelled without prejudice).

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II. AMENDMENTS

Claims 16-42 have been cancelled without prejudice in response to a Restriction/Election

requirement.

III. RESTRICTION REQUIREMENT

The Examiner has required that the claims be restricted to one of the following groups:

Group I, claims 1-15, drawn to an electrochemical fuel cell,

Group II, claims 16-24 & 26, drawn to an air-cooled condenser,

Group III, claim 25, drawn to an evaporatively cooled internally humidified fuel cell,

Group IV, claims 27-40, drawn to a flow field-bipolar plate, and

Group V, claims 41-42, drawn to a method of delivering gas to a fuel cell.

Applicants hereby elect, without traverse, to prosecute claims 1-15, i.e., the Group I

claims. Applicants reserve the right to prosecute the non-elected claims in divisional or

continuing applications.

IV. ELECTION REQUIREMENT

The Examiner has required that an election be made between two allegedly different

species of fuel cells: those fuel cells specific to flow field-bipolar plate assemblies and fuel cells

that are evaporatively cooled and internally humidified. Applicants elect the species of fuel cells

comprising first and second monolithic electrically conducting flow field-bipolar plate

assemblies. Claims 1-15 read on the elected species.

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The Examiner is invited to contact the undersigned patent agentat 713-787-1558 with any questions, comments or suggestions relating to the referenced patent application.

Respectfully submitted,

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